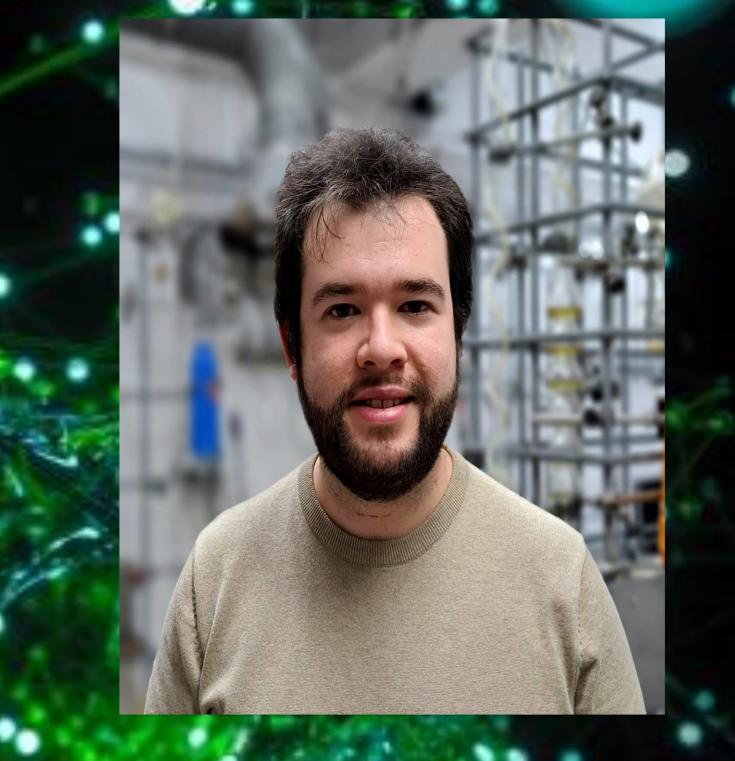


QUEEN'S UNIVERSITY IONIC LIQUID LABORATORIES QUILL





Ionic Liquid Synthesis of Catalysts for Direct CO, Hydrogenation to Short Chain Hydrocarbons

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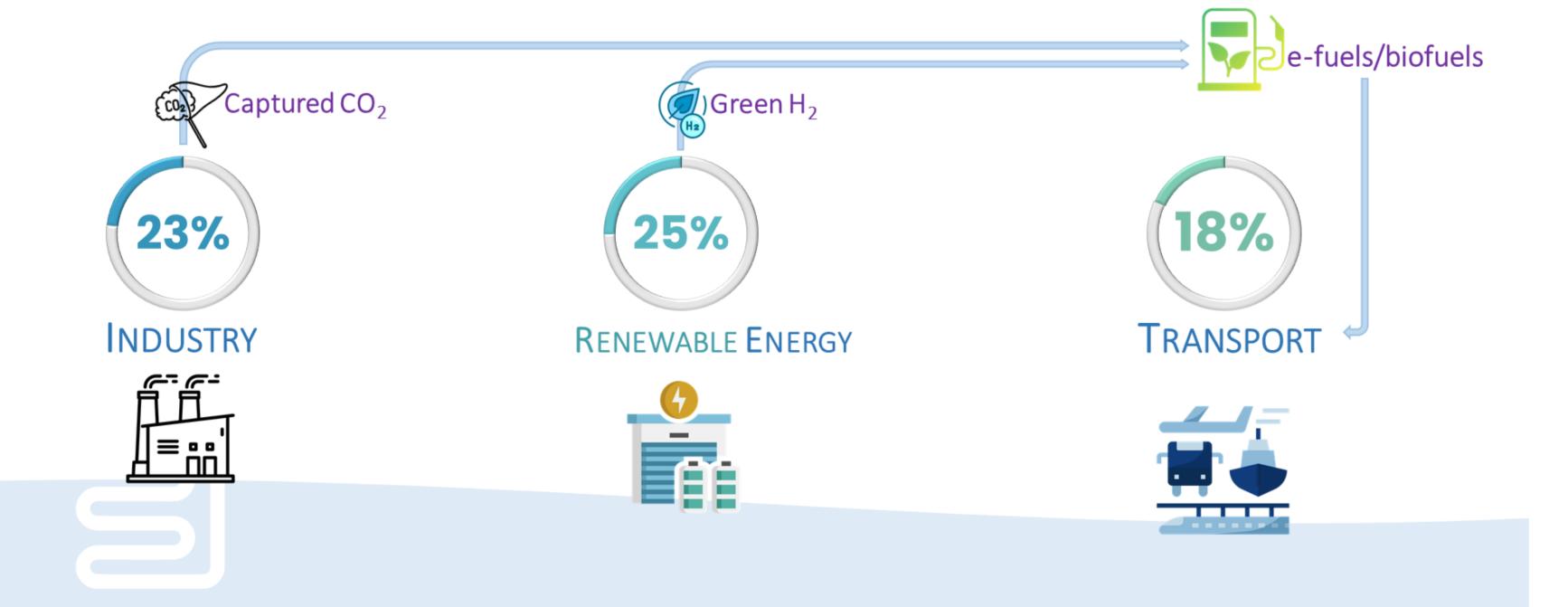
¹CEEP Laboratory, Department of Civil Engineering, Architecture, Territory, Environment and Mathematics, University of Brescia, via Branze 38, 25 I 23 Brescia, Italy; ²School of Chemistry and Chemical Engineering, Queen's University Belfast, David-Keir Building, Stranmillis Road, Belfast, BT9 5AG, UK

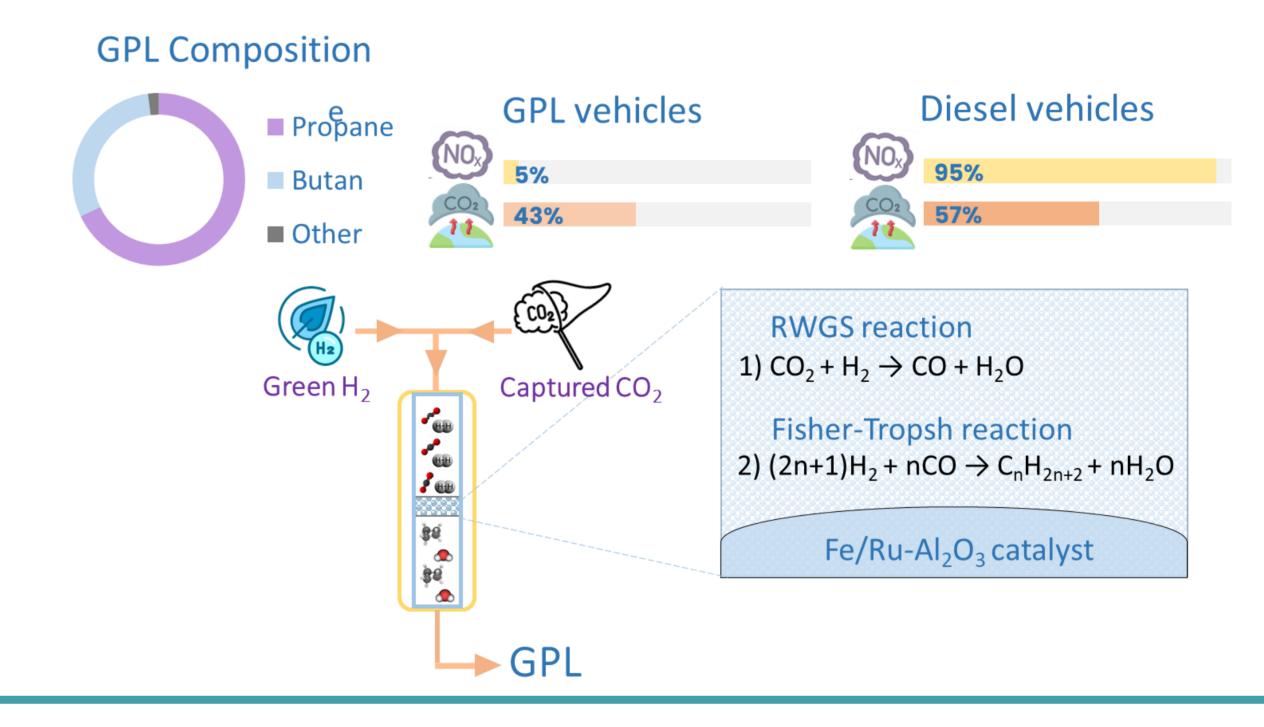
ABSTRACT

The direct conversion of carbon dioxide into lower olefins (C₂-C₄) is a highly desirable process as a sustainable production route¹. These lower olefins, such as ethylene, propylene, and butanes, are crucial components in the chemical industry and for Liquefied Petroleum Gas (LPG). The reaction proceeds via two main consecutive reactions: Reverse Water Gas Shift (RWGS) to produce CO followed by the further conversion of CO to hydrocarbons via the Fischer-Tropsch reaction². Recent studies³ highlight the cost-effectiveness and satisfactory performance of Fe-based catalysts in both reaction steps, while exploring bimetallic catalysts, particularly Ru and Fe combinations, to enhance olefin selectivity⁴, with precise metal nanoparticles (MNP) synthesis as a crucial factor for performance control.

OBJECTIVE

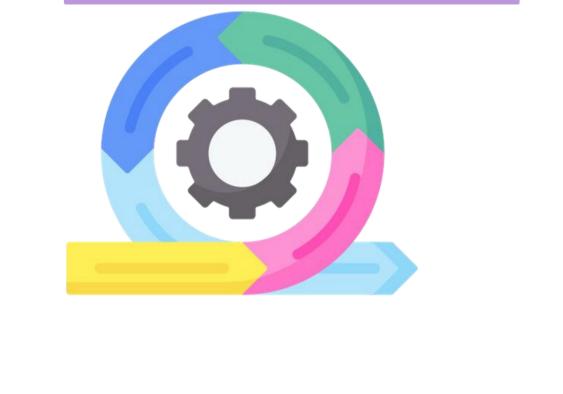
The study introduces a novel approach for synthesizing iron-ruthenium bimetallic catalysts that utilizes ionic liquids as solvents, ensuring precise and uniform distribution of active metal phases. Advanced characterizations and extensive tests reveal that this method surpasses traditional colloid-based techniques, resulting in superior selectivity for target hydrocarbons.



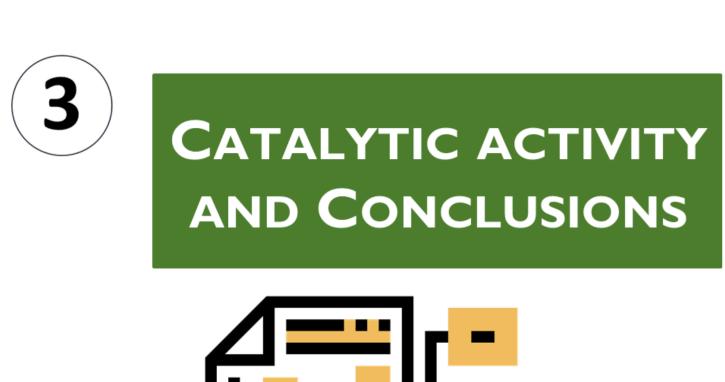


ONIC LIQUID SYNTHESIS



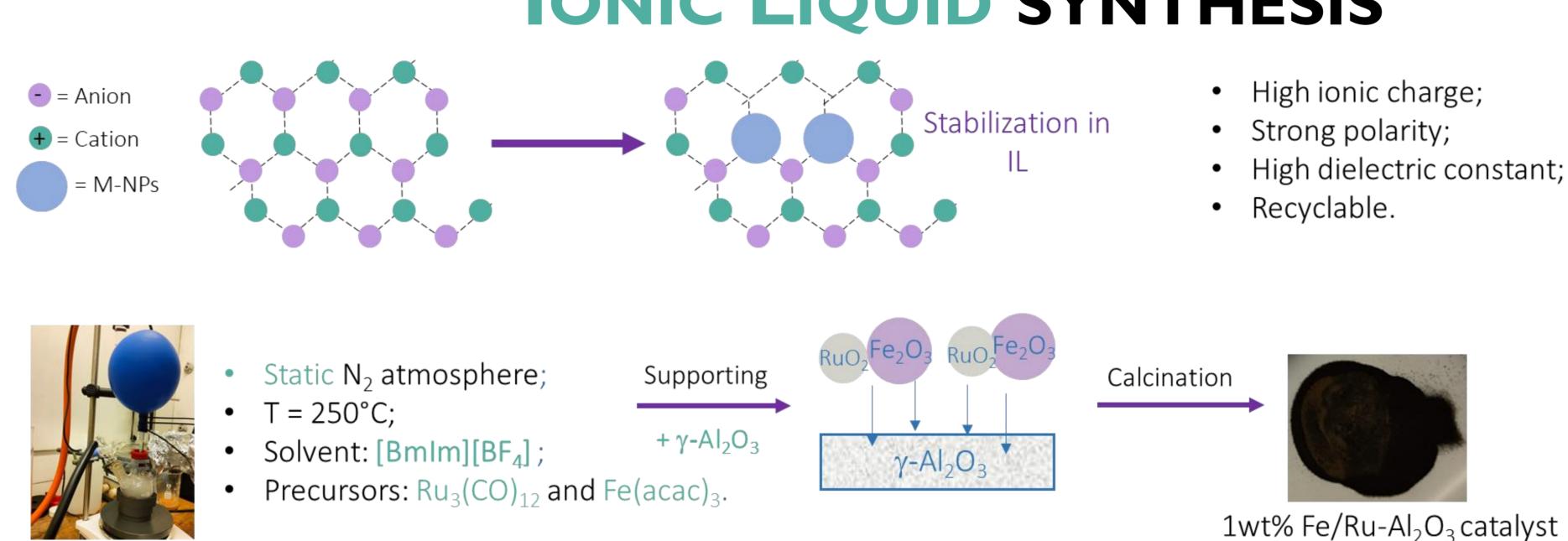


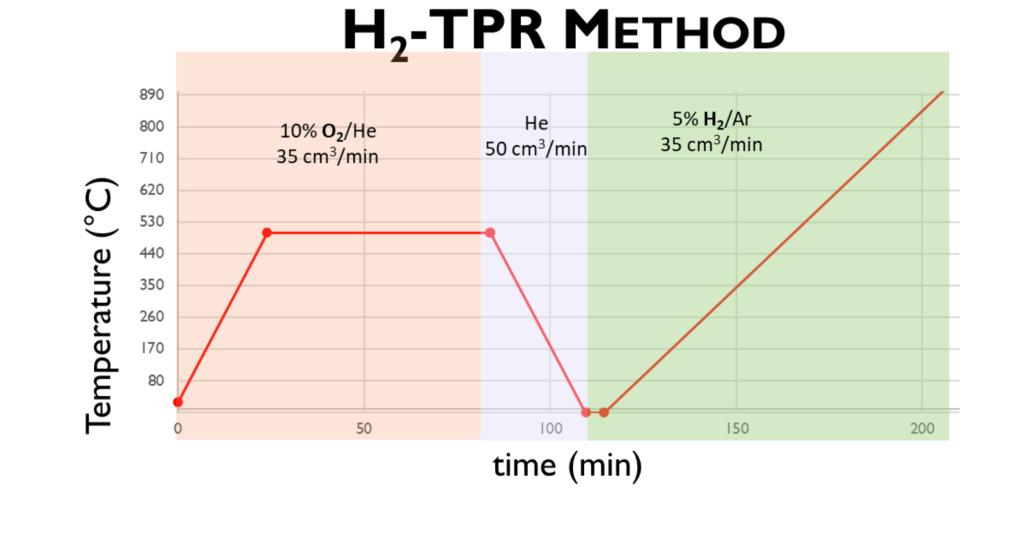


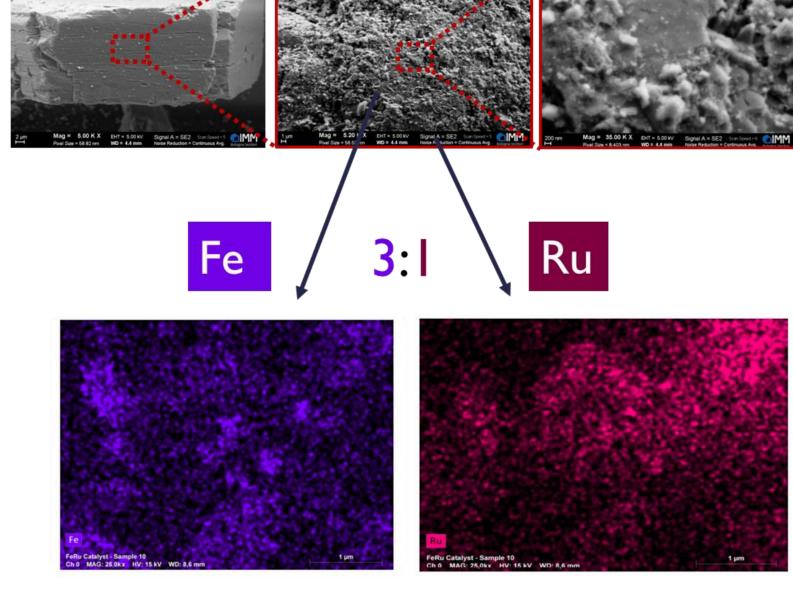












1 μm

200 nm

Figure 1. SEM-EDX analysis of the 1wt% Fe-Ru $3:1/Al_2O_3$ (IL) sample.

C2-C5 CO₂ conversion

Catalyst Name Surface Area Pore Size XRF (wt. %) (Å) (m^2/g) 1 wt.% Fe-Ru 1:1/Al₂O₃ (COL) Fe 0.57 Ru 0.67 88.46 1 wt.% Fe-Ru 3:1/Al₂O₃ (COL) 86.81 Fe 0.7 Ru 0.27 109.44 1 wt.% Fe-Ru 9:1/Al₂O₃ (COL) Fe 1.13 Ru 0.10 90.17 Fe 0.6 Ru 0.7 1 wt.% Fe-Ru 1:1/Al₂O₃ (IL) 86.14 97.34 1 wt.% Fe-Ru 3:1/Al₂O₃ (IL) 93.79 Fe 0.98 Ru 0.29 112.23 91.72 1 wt.% Fe-Ru 9:1/Al₂O₃ (IL) Fe 0.88 Ru 1

Table 1. BET and XRF results of prepared catalysts.

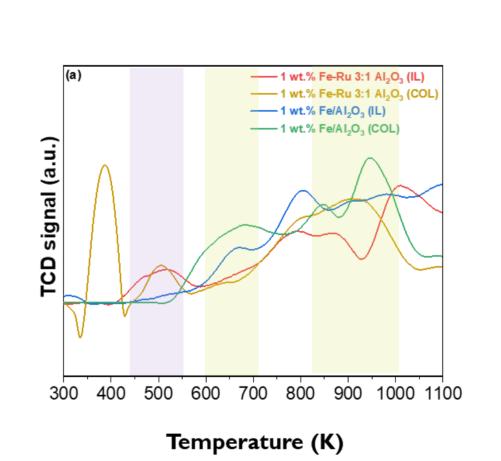


Figure 2a. TPR profiles of Fe-Ru $3:1/Al_2O_3$ catalysts prepared by IL and COL methods

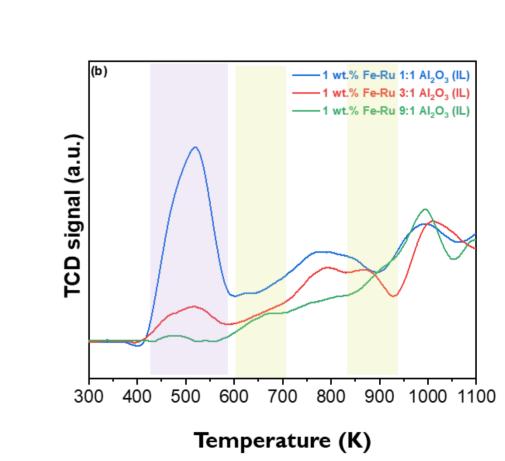


Figure 2b. Comparison of the TPR profiles of 1wt% Fe-Ru/Al₂O₃ (IL) catalysts at three Fe ratios (1:1, 3:1, and 9:1).

CATALYTIC ACTIVITY

 Ionic liquids like [BmIm][BF₄] are used to synthetize bifunctional Fe-Ru catalysts for direct CO₂ conversion to LPG.

CONCLUSIONS

- SEM-EDX shows uniform Fe and Ru NP distribution on Al₂O₃ support.
- XRF confirms near-theoretical metal loadings with the desired Fe/Ru ratio. The study shows IL synthesis improves catalyst reducibility and Fe-Ru interaction.
- Preliminary catalytic tests at 20 bar and 45 mL/min indicate that variations in reducibility align with catalytic activity differences.
- IL-prepared catalysts show a fivefold increase in CO₂ conversion to LPG hydrocarbons compared to COL-prepared ones.

M. Maddaloni, A. Centeno-Pedrazo, S. Avanzi, N. J. Mazumdar, H. Manyar, N. Artioli, Catalysts, 2023, 13, 1499

ACKNOWLEDGMENT

<u>2</u> μm

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